



# New exploratory testing conditions to understand the gas transfer mechanisms through VIPs' barriers

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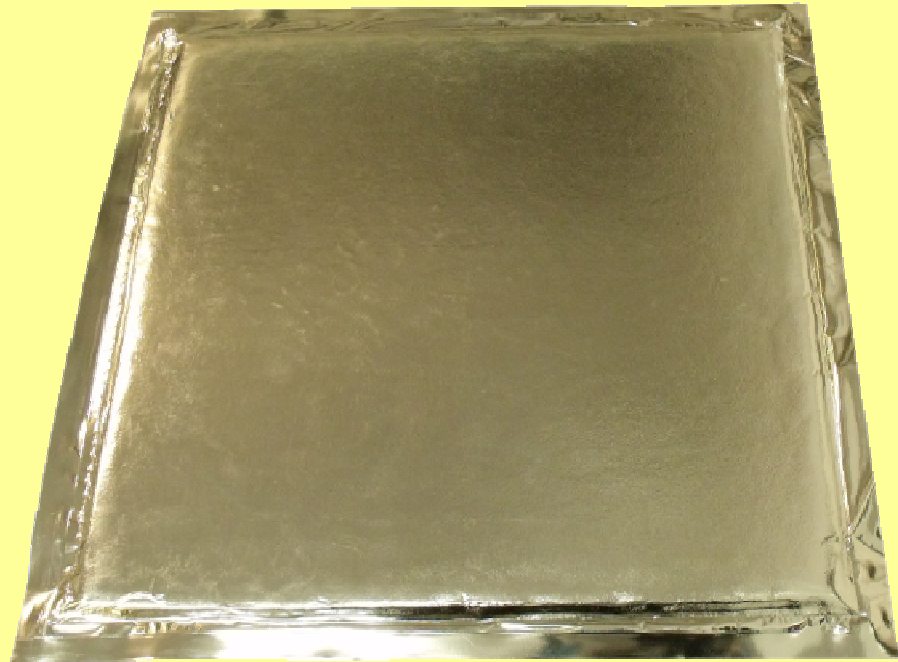
I. Introduction

II. Gas permeation through VIP  
barrier envelop: modeling

III. New exploratory conditions for  
gas permeation measurements

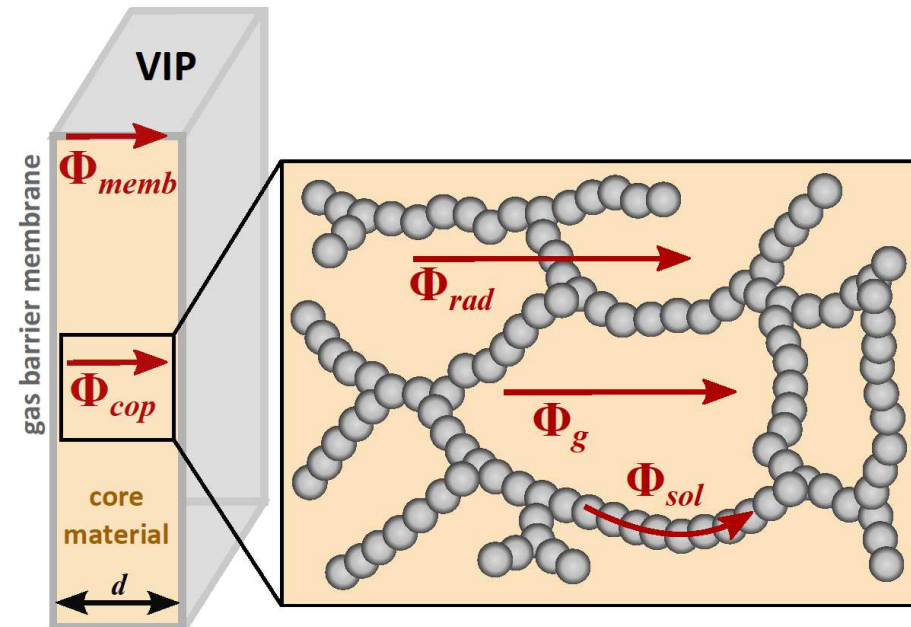
IV. Conclusion & outlook

# I. Introduction: VIP thermal performance & aging



# Thermal performance of VIPs: parallel fluxes model

- Heat fluxes in the core material:
    - Radiative heat transfer  $\Phi_{rad}$
    - Solid conduction  $\Phi_{sol}$
    - Gaseous heat transfer  $\Phi_g$
  - Thermal bridge through the edge (gas barrier membrane)  $\Phi_{memb}$
  - Parallel fluxes
  - Independent fluxes
- Elementary conductivities can be summed



$$\lambda_{tot} = \lambda_{rad} + \lambda_{sol} + \lambda_g + \lambda_{memb}$$

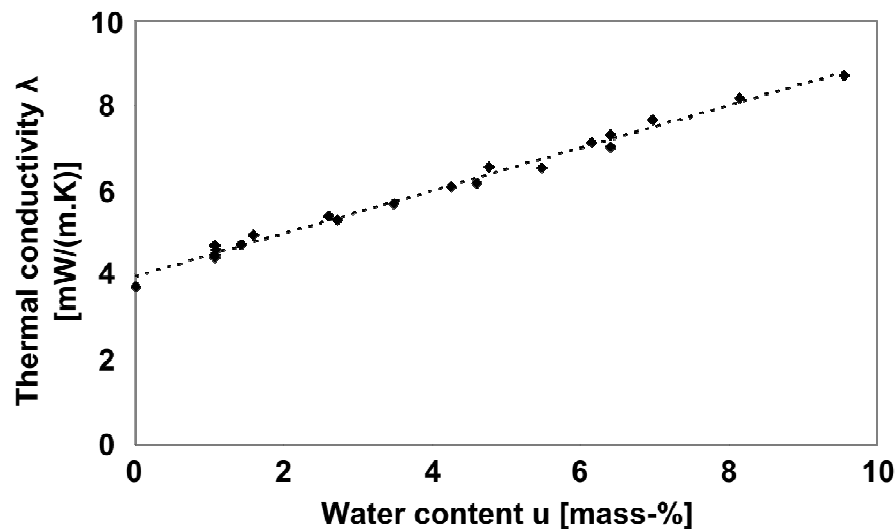
dry core / moisture

$$\lambda_{tot} = \lambda_{rad} + (\lambda_{sol,dry} + \lambda_u) + \lambda_g + \lambda_{memb}$$

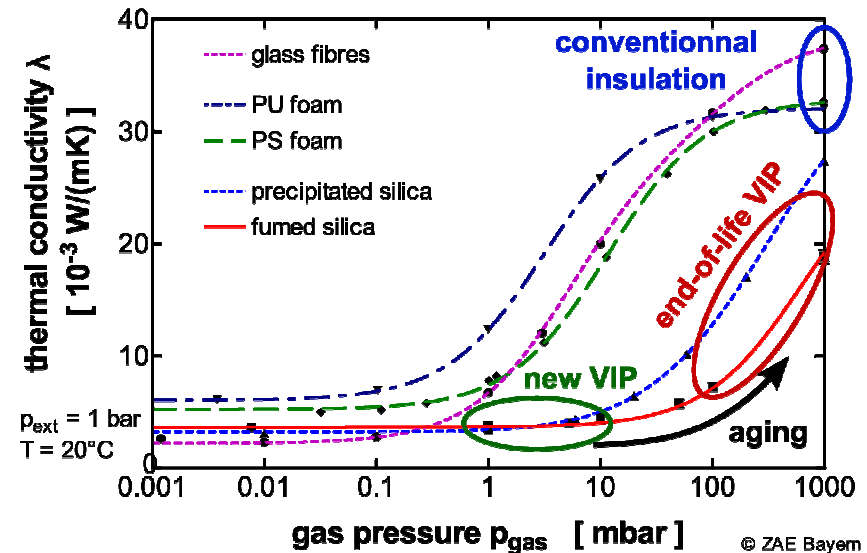
# Thermal performance of VIPs: parallel fluxes model 2/2

$$\lambda_{tot} = \lambda_{rad} + (\lambda_{sol,dry} + \lambda_u) + \lambda_g + \lambda_{memb}$$

$\lambda_{rad} \approx 1 \text{ mW}/(\text{m.K})$   
 $\lambda_{sol} \approx 3 \text{ mW}/(\text{m.K})$   
 $\lambda_u \approx 0 - 3 \text{ mW}/(\text{m.K})$   
 $\lambda_g \approx 0 - 15 \text{ mW}/(\text{m.K})$   
 $\lambda_{memb} \approx 1 \text{ mW}/(\text{m.K})$



[IEA Annex 39, 2005]



[IEA Annex 39, 2005]

## Thermal performance & aging mechanism

$$\lambda_{tot} = \lambda_{rad} + (\lambda_{sol,dry} + \lambda_u) + \lambda_g + \lambda_{memb}$$

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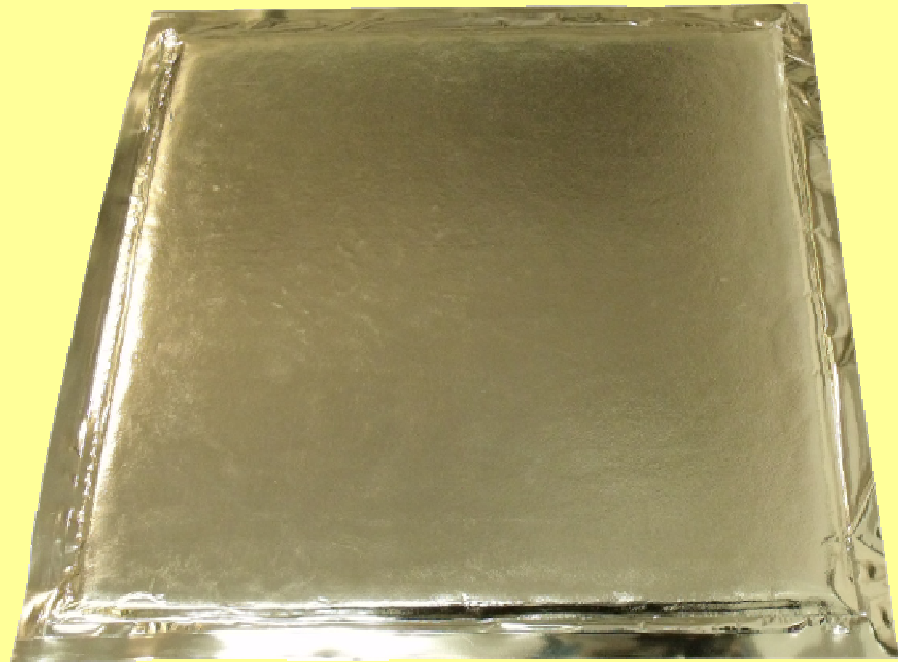
$\lambda_{memb} \approx 1 \text{ mW}/(\text{m.K})$

Core material water content  $u = f_1(t)$

Internal pressure  $p = f_2(t)$

- The gas permeation through VIP envelopes should be quantified for the prediction of the thermal performance over the whole lifetime
- Dry air and water vapor should be quantified separately (not the same impact)

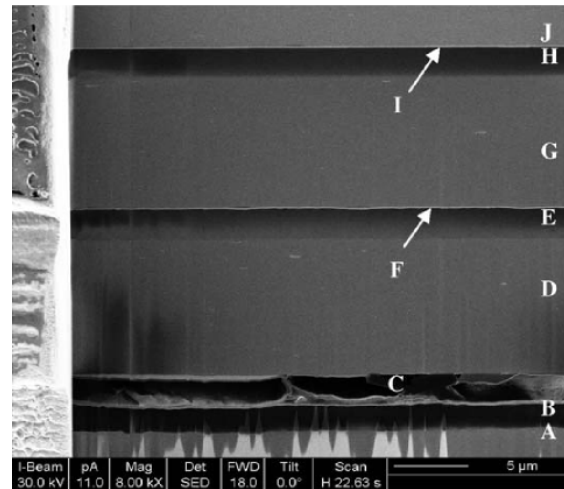
## II. Gas permeation through VIP barrier envelop: modeling



# State-of-the art gas permeation modeling

## Multilayer membrane scale

[BRUNNER et al, Surface & Coatings Technology, vol 200, 2006]



J	PET	Polyethylene terephthalate	12 µm
I	AL	Aluminium	100 nm = 0.1 µm
H	PU	Polyurethane	2 µm
G	PET	Polyethylene terephthalate	12 µm
F	AL	Aluminium	100 nm = 0.1 µm
E	PU	Polyurethane	2 µm
D	PET	Polyethylene terephthalate	12 µm
C	AL	Aluminium	100 nm = 0.1 µm
B	PU	Polyurethane	2 µm
A	LDPE	Low Density Polyethylene	50 µm

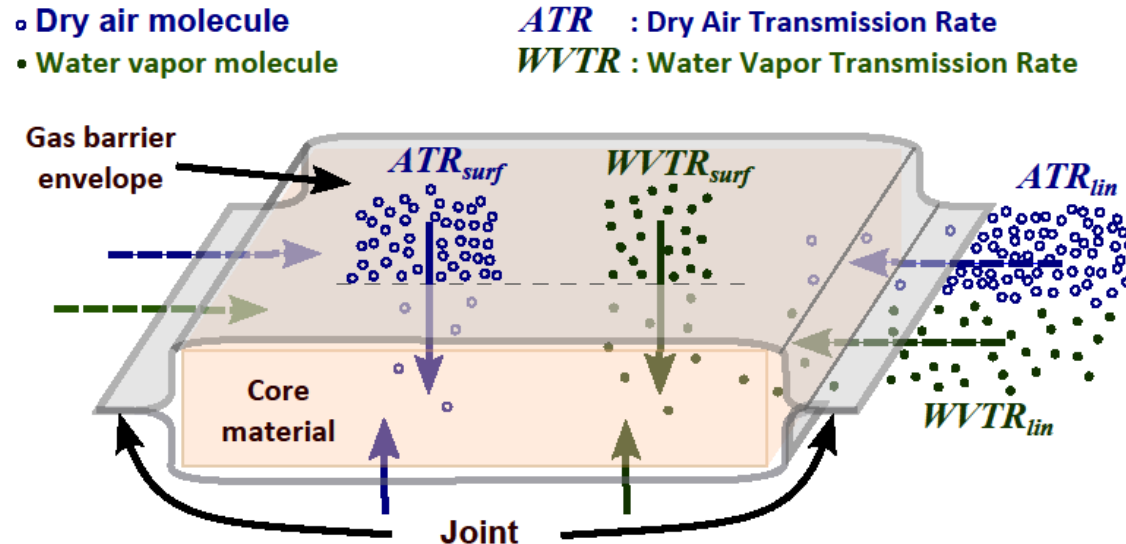
- At multilayer membrane scale: Sorption-Diffusion model (SD model)
  - Partial pressure gradient  $\Delta p_i$  is the driving force for gas transmission

$$GTR_{surf} = \Pi_{surf} \Delta p_i$$

- Permeance  $\Pi$  is temperature dependant

$$\Pi_i = \Pi_i^0 \exp(-E_a/RT)$$

# State-of-the art gas permeation modeling VIP scale



- At whole VIP scale: 4 contributions to gas transfer
  - Two locations (faces & edges)
 
$$ATR_{tot} = A \cdot ATR_{surf} + P \cdot ATR_{lin}$$

$$WVTR_{tot} = A \cdot WVTR_{surf} + P \cdot WVTR_{lin}$$
  - Two gases (dry air and water vapor)
 
$$GTR_{tot} = ATR_{tot} + WVTR_{tot}$$

- Final expression of water vapor or dry air permeation rate

$$ATR_{tot} = A \cdot \Pi_{air,surf} \cdot \Delta p_{air} + P \cdot \Pi_{air,lin} \cdot \Delta p_{air}$$

$$WVTR_{tot} = A \cdot \Pi_{vap,surf} \cdot \Delta p_{vap} + P \cdot \Pi_{vap,lin} \cdot \Delta p_{vap} \quad 9$$

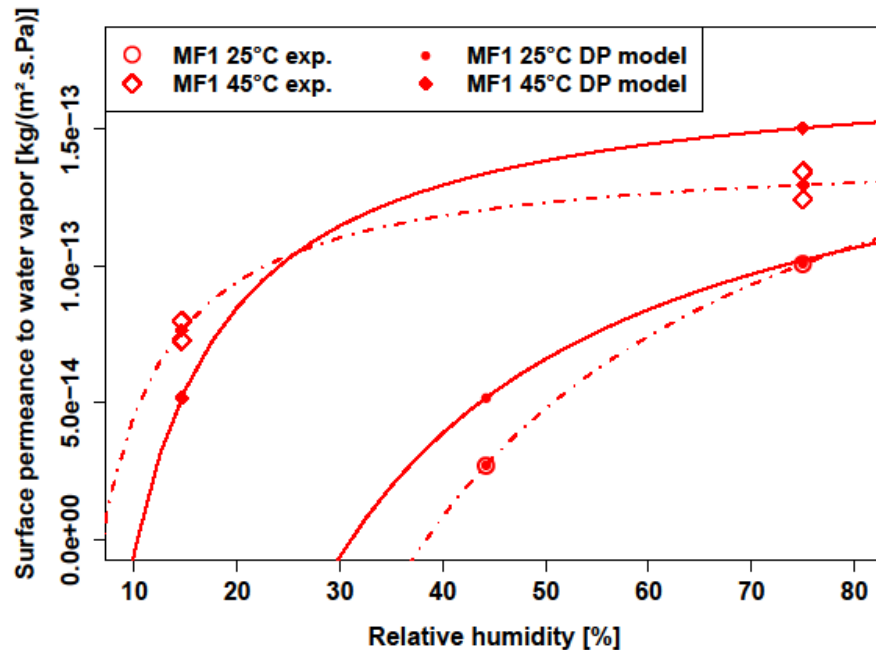
## Alternative permeation model: Dual Pressure model



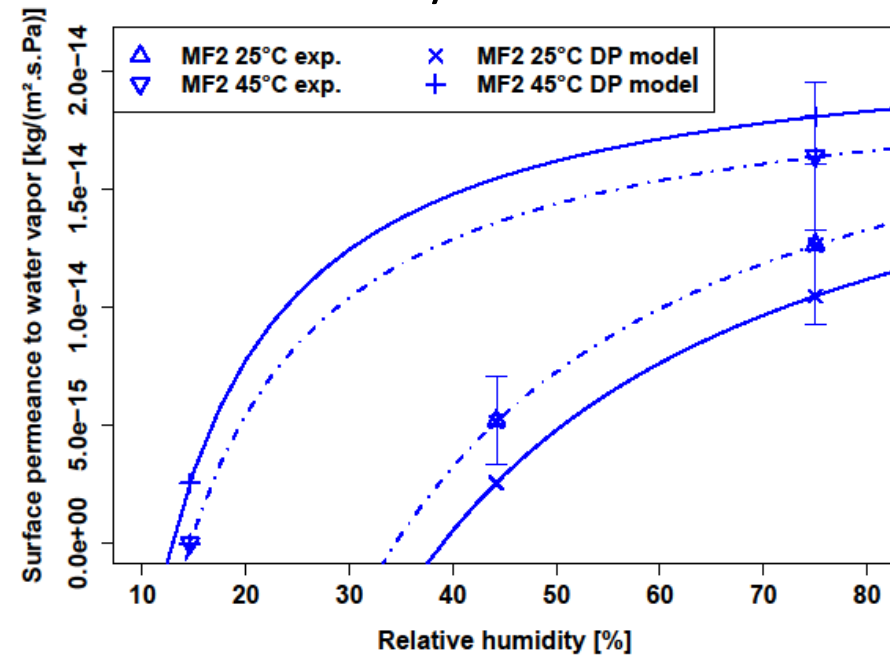
- Arguments in favor of a coupled model for mass transfer
  - Thermodynamics of irreversible processes
  - Competition or cooperation between gas components for sorption and diffusion
  - Influence of relative humidity on dry air transmission rates
- Alternative model proposed: the Dual Pressure model (DP)
  - Takes into account partial pressure gradient  $\Delta p_i$  and the total pressure gradient  $\Delta p_{tot}$
  - Gas transmission rate: 
$$GTR_{surf} = K_1 \Delta p_i + K_2 \Delta p_{tot}$$
  - Apparent permeance: 
$$\Pi_{surf} = -\frac{GTR_{surf}}{\Delta p_i} = K_1 + K_2 \frac{\Delta p_{tot}}{\Delta p_i}$$
- Coefficients  $K_1$  et  $K_2$  can be identified on exp. data from IEA Annex 39 (VIP aging in climatic rooms)

# Water vapor surface permeances from the DP model

## Multilayer Barrier 1

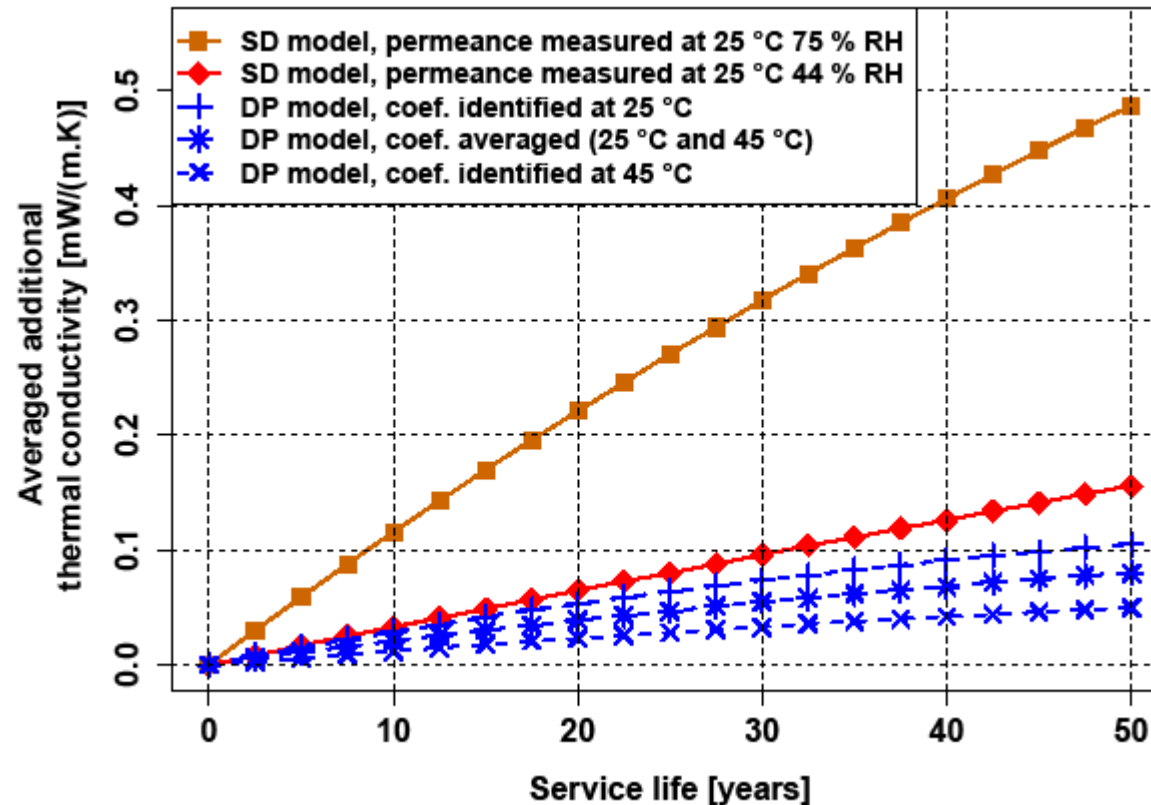


## Multilayer Barrier 2



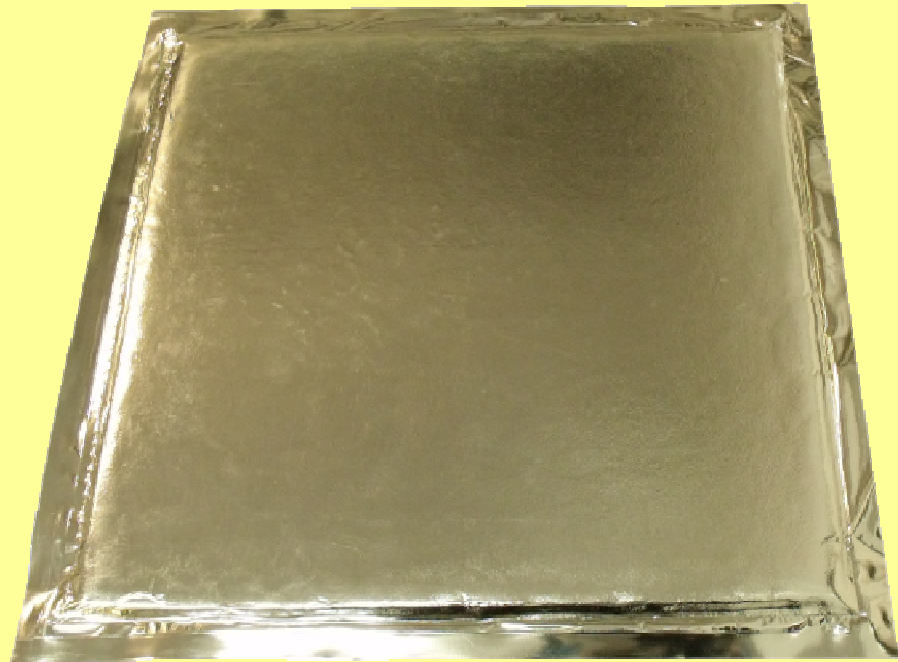
- Dotted lines: the parameter set ( $K_1$ ,  $K_2$ ) is identified at each temperature
- Solid lines: the parameter set ( $K_1$ ,  $K_2$ ) is averaged over all temperatures

## Model behaviors: Sorption-diffusion (SD) vs. dual pressure (DP)



- $\Pi$ ,  $K_1$  and  $K_2$  identified on exp. data from IEA Annex 39
- Climatic conditions during service:  $T = 25\text{ °C}$ ,  $\varphi = 44\%$
- DP model less sensitive to experimental conditions identification

### III. New exploratory conditions for gas permeation measurements



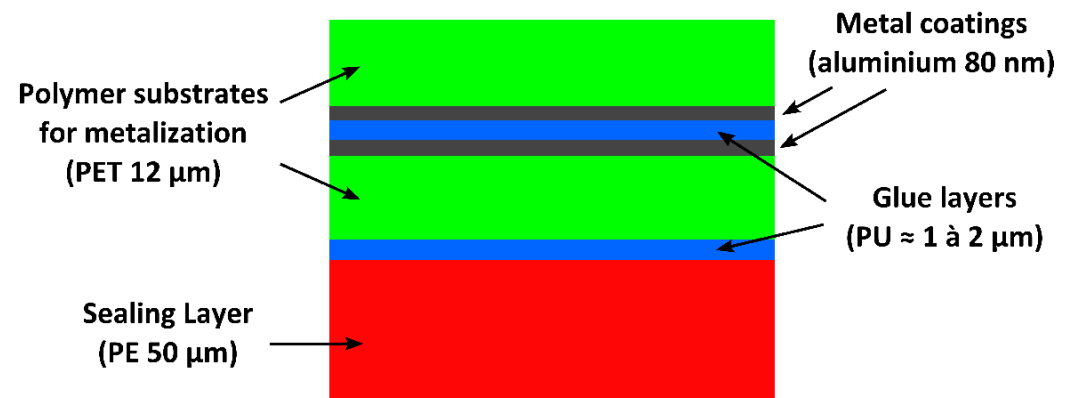
## Exploratory experimental plan in new conditions

- Goal: to measure the influence of the water vapor molar concentration, at constant water vapor partial pressure → influence of the total pressure ?

Condition	Temperature $T$ [°C]	Relative humidity $\phi$ [%]	Total pressure $p_{tot}$ [Pa]	Water vapor molar concentration $X_{vap}$ [%]
1	48	65 %	7 270	100 %
2	48	65 %	24 000	30 %
3	48	65 %	100 000	7 %

- Two experimental methods:
  - Manometric method: measurement of the pressure increase
  - VIP aging in climatic rooms: measurement of the mass increase

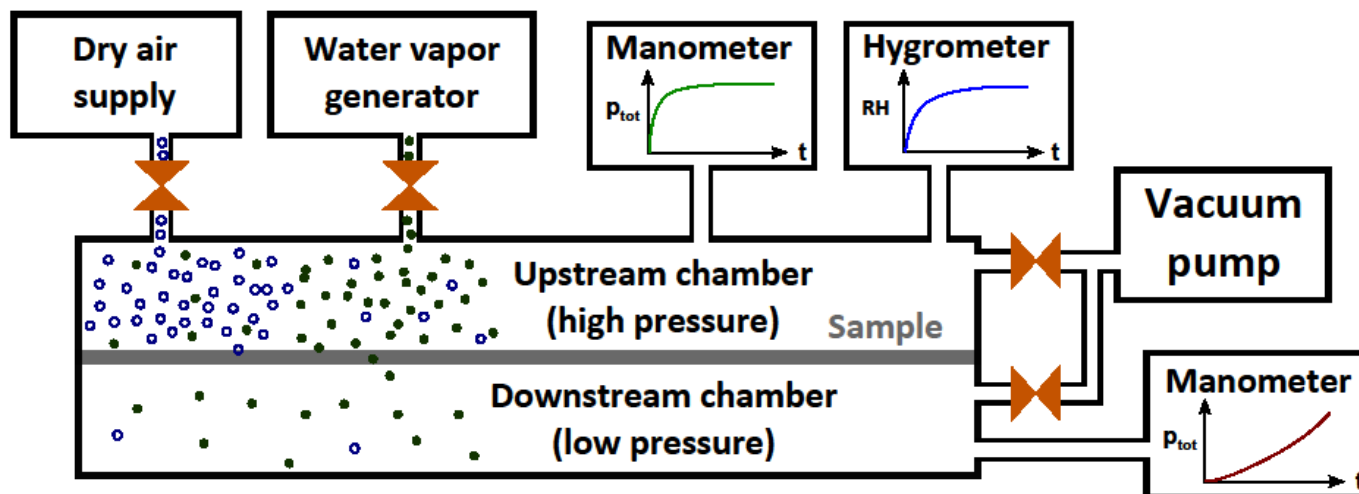
- Membrane MF8 : bilayer of an Al-coated PET (12  $\mu\text{m}$  PET + 80 nm Al) + sealing layer PE 50  $\mu\text{m}$



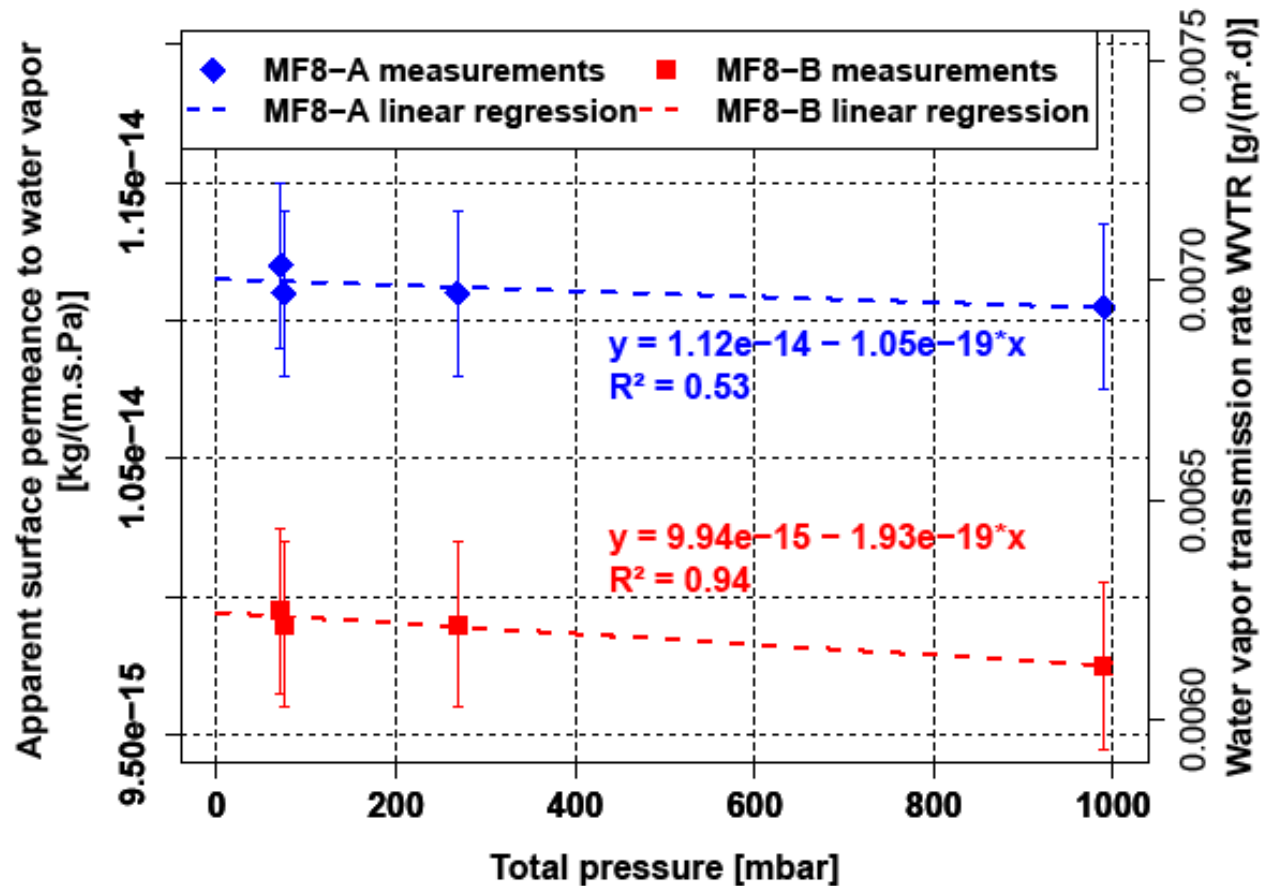
## Experimental method 1: Manometric method at the scale of the barrier membrane



- Humid air configuration (modified “Deltaperm” device)
  - Upstream chamber : mixture of water vapor + dry air
  - Hard to measure the dry air transmission rate  $ATR \approx 100$  times lower than WVTR
  - The whole gas transmission rate  $GTR$  is measured, it is assimilated to the water vapor transmission rate  $WVTR$  (air transmission rate  $ATR$  negligible)



# Manometric method measurements in humid air configuration: surface permeance to water vapor



- Very slight influence of the total pressure: total variation < 2 %

## Experimental method 2: whole VIP scale Accelerated gas permeation

- Accelerated aging of VIPs in climatic rooms, at high temperature & humidity



- Raw measurement data: mass and pressure increase over time
- What is needed for accurate measurements ?
  - Accurate measurements of core material hygroscopic properties
  - Good control of climatic conditions (temperature, RH, total pressure)
  - Large number of samples with various perimeter / area ratios
  - Combined measurement of mass and pressure increase
  - Long measurement period for stabilization (several weeks)

## Accelerated VIP aging measurements: Surface and linear permeance to water vapor

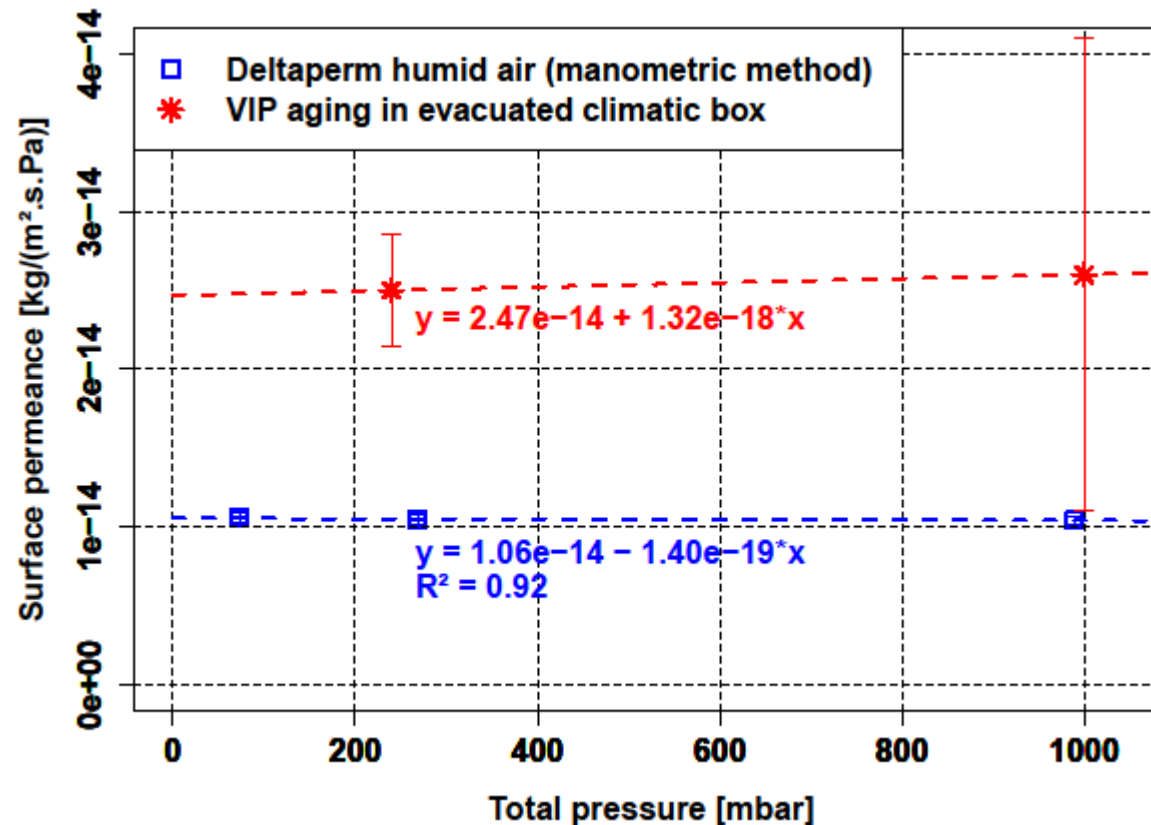


Membrane and experimental condition	Total pressure $p_{tot}$ [mbar]	Surface permeance $\Pi_{surf}$ [kg/m <sup>2</sup> .s.Pa]	Linear permeance $\Pi_{lin}$ [kg/m.s.Pa]
MF8 / Condition 2	240 mbar	$2,5 \times 10^{-14} \pm 4 \times 10^{-15}$	$9,2 \times 10^{-16} \pm 10^{-15}$
MF8 / Condition 3	1 000 mbar	$2,6 \times 10^{-14} \pm 1,5 \times 10^{-14}$	$2,7 \times 10^{-15} \pm 3 \times 10^{-15}$
MF2 (IEA Annex 39) $T = 45^{\circ}\text{C}$ et $\varphi = 75\%$ HR	1 000 mbar	$1,6 \times 10^{-14}$	$3 \times 10^{-15}$

- The influence of the total pressure on the surface permeance seems to be negligible
- The linear permeance seems to be an increasing function of the total pressure

Membrane	Linear permeance to water vapor $\Pi_{lin,vap}$ [kg/m.s.Pa]	Linear permeance to dry air $\Pi_{lin,air}$ [kg/m.s.Pa]
MF8	$5,2 \times 10^{-16}$	$1,7 \times 10^{-16}$
MF2 (IEA Annex 39)	$3 \times 10^{-15}$	$8 \times 10^{-19}$

## Experimental results: surface permeance to water vapor from both measurement methods



- Influence of the total pressure: negligible for both methods
- Influence of the method: factor 2.5 for the same barrier membrane

## Influence of the total pressure



$$\Pi_{vap} = K_{1,vap} + K_{2,vap} \frac{\Delta p_{tot}}{\Delta p_{vap}} = K_{1,vap} \left( 1 + \frac{K_{2,vap}}{K_{1,vap} X_{vap}} \right)$$

- Experimental data from IEA Annex 39

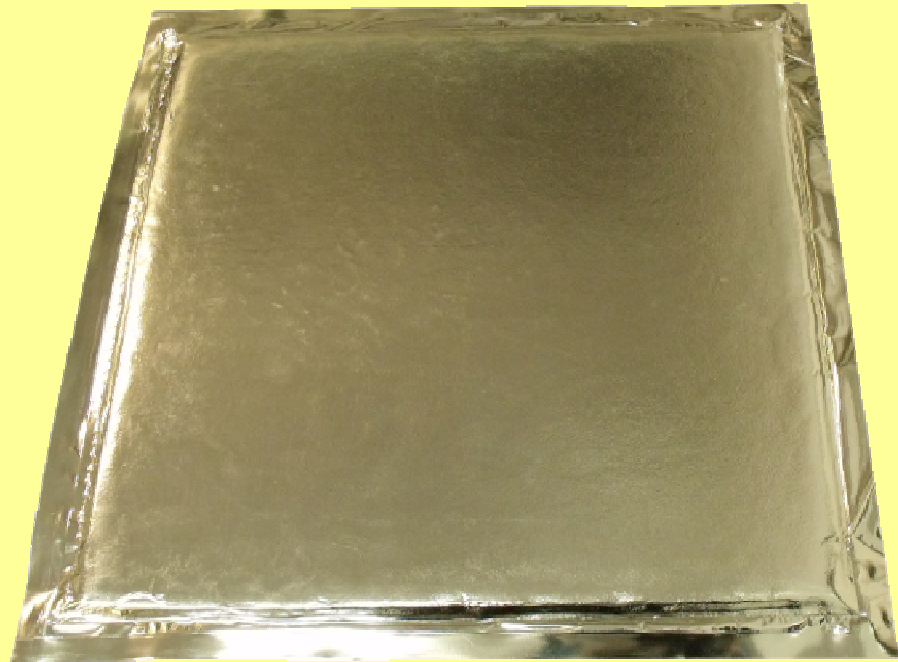
$$\frac{K_{2,vap}}{K_{1,vap}} \approx -0,01 \quad \& \quad X_{vap} \in [1,4\% - 7,2\%] \quad \rightarrow \quad \frac{K_{2,vap}}{K_{1,vap} X_{vap}} \in [14\% - 70\%]$$

- Experimental conditions used here:  $T = 48 \text{ }^{\circ}\text{C}$ ,  $\phi = 65 \text{ \% HR}$

$$\frac{K_{2,vap}}{K_{1,vap}} \approx -0,001 \quad \& \quad X_{vap} \in [7,2\% - 100\%] \quad \rightarrow \quad \frac{K_{2,vap}}{K_{1,vap} X_{vap}} \in [0,1\% - 1,4\%]$$

- The influence of the total pressure may still exist, but may not be measurable in our conditions  
 $\rightarrow$  Dry conditions experiments required to estimate the potential influence

# IV. Conclusion



## Conclusion

Main aging phenomenon: **gas permeation through VIP envelopes**

→ Sorption-Diffusion model as a reference model, partial pressure as transfer driver



**Alternative model for mass transfer: Dual Pressure model (DP)**

Takes into account both *partial pressure* and *total pressure*

→ Both models are consistent with existing experimental data (but not extensive)



Need for new experiments: *influence of the total pressure ?*

→ **Two methods** for exploratory experimental plan

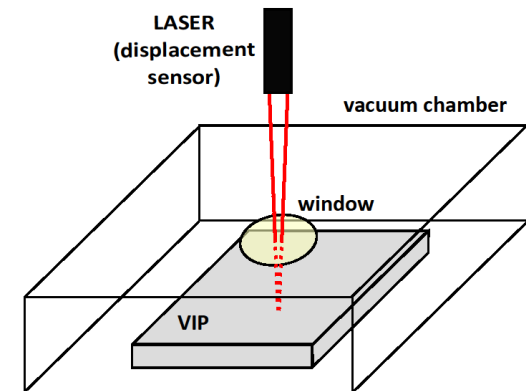


### Experimental results

- No influence of the total pressure on surface permeance → exp. conditions ?
- Influence of the total pressure on linear permeance → uncertainty and air / vapor
- Influence of the method → sample integrity // sample size

## *Three main matters for experimental exploration:*

- Influence of the total pressure on **surface permeance** (VIPs' faces)
  - Dual pressure model for **moderate temperature and humidity**:
  - Measurements over **long periods** with **high precision balance**
- Influence of the total pressure on **linear permeance** (VIPs' edges)
  - Accuracy of VIP aging measurements: **high precision balance** and **long periods**
  - **Internal pressure measurement** through the lift-off procedure
- Influence of the experimental method: where does the factor 2.5 come from ?
  - **Envelope sample integrity** after VIP manufacturing ? (samples from manufactured VIP)
  - Sample size and selection → long term measurements on small VIPs
  - Other causes: influence of the gas mixture on the low pressure side



Thanks for your attention !